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the vinyl chloride are introduced into an organic solvent consisting of at least one saturated halogen-containing hydrocarbon.

2. (Amended) The [P]process according to Claim 1, wherein the saturated halogen-containing hydrocarbon is selected from chloro-, fluoro- or chlorofluorohydrocarbons containing from 1 to 8 carbon atoms.

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3. (Amended) The [P]process according to Claim 2, wherein the saturated halogen-containing hydrocarbon of the process is used as solvent.

4. (Amended) The [P]process according to Claim 1, wherein the reaction mixture contains, at all times, at least 55% by weight of solvent.

5. (Amended) The [P]process according to Claim 1, wherein the introduction of the vinyl chloride and hydrogen fluoride is controlled so that, at all times, the vinyl chloride content is less than 15% and that of hydrogen fluoride is less than 30% of the weight of the reaction mixture.

6. (Amended) The [P]process according to Claim 1, wherein the molar ratio between the hydrogen fluoride and the vinyl chloride used is at least 1 and does not exceed 20.

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7. (Amended) The [P]process according to Claim 1, wherein the reaction is carried out in the presence of a hydrofluorination catalyst chosen from derivatives of metals of groups IIIa, IVa, IVb, Va, Vb and VIb of the Periodic Table of the elements, and their mixtures.

8. (Amended) The [P]process according to Claim 1, wherein the reaction is performed at a temperature of at least 40° and not exceeding 130°C and at a pressure at least equal to 2 bar and not exceeding 50 bar.

9. (Amended) The [P]process according to Claim 1, wherein the [desired] product is withdrawn continuously from the reaction mixture.

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10. (Amended) The [P]process according to Claim 9, wherein the product is [applied to the production of] 1,1-difluoroethane, [wherein it] which is withdrawn in gaseous form.